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الراعي الرسمي



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KNPC EFFORTS TOWARDS REDUCING HYDROCARBON LOSS & FLARE GAS MANAGEMENT



- ⑩ Introduction.
- ⑩ Challenges
- ⑩ Efforts Made:
 - ⑩ Review the measurement methodology :
losses type, Source , measurement & breakdown
 - ⑩ Defining the uncertainties.
 - ⑩ reconciliation method & Correction factors
- ⑩ Conclusion

Introduction

- ⑩ KNPC Operates highly complex Refineries.
 - ⑩ Complex units & integration
 - ⑩ Thousands of valves flowmeters & analyzers
 - ⑩ More than 20 Elevated Flare Stacks

- ⑩ Current Capacity over 700,000 BPD

Challenges



⑩ In 2015, High hydrocarbon loss (by balance) reported.

Refinery Loss (loss by balance) = Refinery input –
Refinery output – Fuels + (Δ Inventory).

⑩ The same was captured by SAB & raised in the
parliament.

Efforts Made

- ⑩ committee formed to review accounting methodologies & practices being followed.
- ⑩ Defining the losses type, Source breakdown, accounting Methodologies
- ⑩ Defining the uncertainty reasons.
- ⑩ Defining the correction factors

Finding :



Loss Types:

- ⑩ **Controllable loss** : Losses that can be reduced to the bench mark levels based on the refinery configuration.

- ⑩ **Non-Controllable loss** : Losses that is part of normal refinery operation (i.e. side products or side loss)

Finding:



Controllable Losses	Breakdown	Measurement Method	Reference
H/c loss through Flares (Ex H2)	13%	<i>Flowmeters</i>	Chevron feedback , International Standards
H/c loss to Bio-treatment	6%	Analysis + Calculation	Newly Identified , IP Document Page 34
H/C in Sea Water effluent		Analysis + Calculation	Record Available , to be reported
API Evaporation & Process Fugitives		Analysis + Calculation	Records available, to be re-classified and reported as per the standards. IP Document Page 8
Hydrogen Venting		Flowmeters	Record Available. To be included in loss report for MAA & MAB

Finding:



Non-controllable Process Losses	Breakdown	Measurement Method	Reference
Carbon loss as CO ₂ from HP Units	71%	Mass Balance, part of production	International Standard IP Doc Page 34 & Solomon Methodology
H ₂ loss as H ₂ O from SRU Units	10%	Mass Balance, part of production	International Standard, IP Doc page 7 Record available to be reported.
Nitrogen Loss as NH ₃		Mass Balance, part of production	International Standard IP Doc Page 34 No record for MAA & SHU.
FCC Coke		Heat Balance	Solomon Methodology
CCR Coke		Heat Balance	Newly Identified found in IP Document page 7
Flare Pilot & Purge		Design figures	Solomon Methodology
VOC Emissions		analysis & calculations	Solomon Methodology
Hydrocarbon in dispatched Ash (WWT) / waste		analysis	Newly Identified , found in IP document Page 9

Defining the uncertainty reasons

⑩ Instrumentation errors

⑩ Test run to ensure instrumentation accuracy.

➤ Systematic error.

➤ Random error.

⑩ Non-hydrocarbon interference.

➤ Analyze the flared gas and deduct the purge gas quantities and the non hydrocarbon gases.

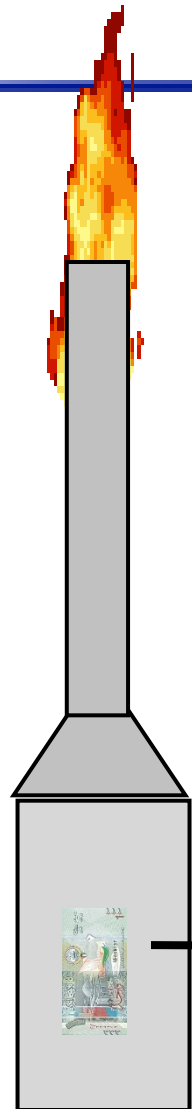
⑩ Zero value losses

➤ Part of the refinery operation.

Reconciliation method & Obtaining Correction factors



- Reconciliation method [link](#)



Passing Sample Point Purge

Passing v/v of De-Pressurizing lines

Passing pump casing vent

Flare header FG Purge

Compressor Suction K.O.D Drain

Passing PSV

Compressor Stuffing Box Lines

Passing Control Valves

Passing Gas Traps

GT





FUP HYDROCARBON FLARE STACK (62-ST-101/102)

NEXT

Unit	Tag. No	Description	Flaring	Value	FLARE INSTRUMENTS SPECIFICATIONS		
					VALUE OPEN %	FLOW RANGE NM ³ /H	High Alarm
FUP Main Flow Meter (A)	62FR104.PV	FUP H/C FLARE 62-ST-101		0.18	-	0-20000	NIL
FUP Main Flow Meter (B)	62FR105.PV	FUP H/C FLARE 62-ST-102		0.26	-	0-20000	NIL
FUP ARD (Unit 81)	81FI323.PV	REACTOR H/C COMM HDR		257.62	-	0-10000	13
	81FI325.PV	FRACT. H/C COMM HDR		54.55	-	0-3000	13
	81FI326.PV	COMP. COMM HDR		752.41	-	0-2000	13
	81PRC077.OP	V-028 FRACT GAS KOD	NO	36.07	50-100	-	NIL
FUP ARD (Unit 82)	82FI323.PV	REACTOR H/C COMM HDR		10003.15	-	0-10000	NIL
HCR (Unit 84)	84FI513.PV	FLARE GAS REACTOR SIDE		-7.52	-	0-5000	50
	84FI514.PV	FLARE GAS FRACTIONATOR		761.36	-	0-2000	1000
	84PC116A.OP	V-110 FEED SURGE DRUM	NO	-5.00	50-100	-	NIL
	84PIC301.OP	V-301 CLPS Off Gas HR/FLARE	Yes	59.84	0-100	-	NIL
	84PIC304.OP	V-320 FRACTIONATOR OVERHEAD	NO	-5.00	50-100	-	NIL

MAIN





Reconciliation method & Obtaining Correction factors

- Obtaining Correction factors
 - Lab analysis.
 - Field survey. [Link](#)
 - Mass Balance.



AccuTrack – a small hand-held device that measures the sound created by gases or liquids passing through an opening.



V-Pac – a much more sophisticated device to measure sound. Can estimate quantity of passing.



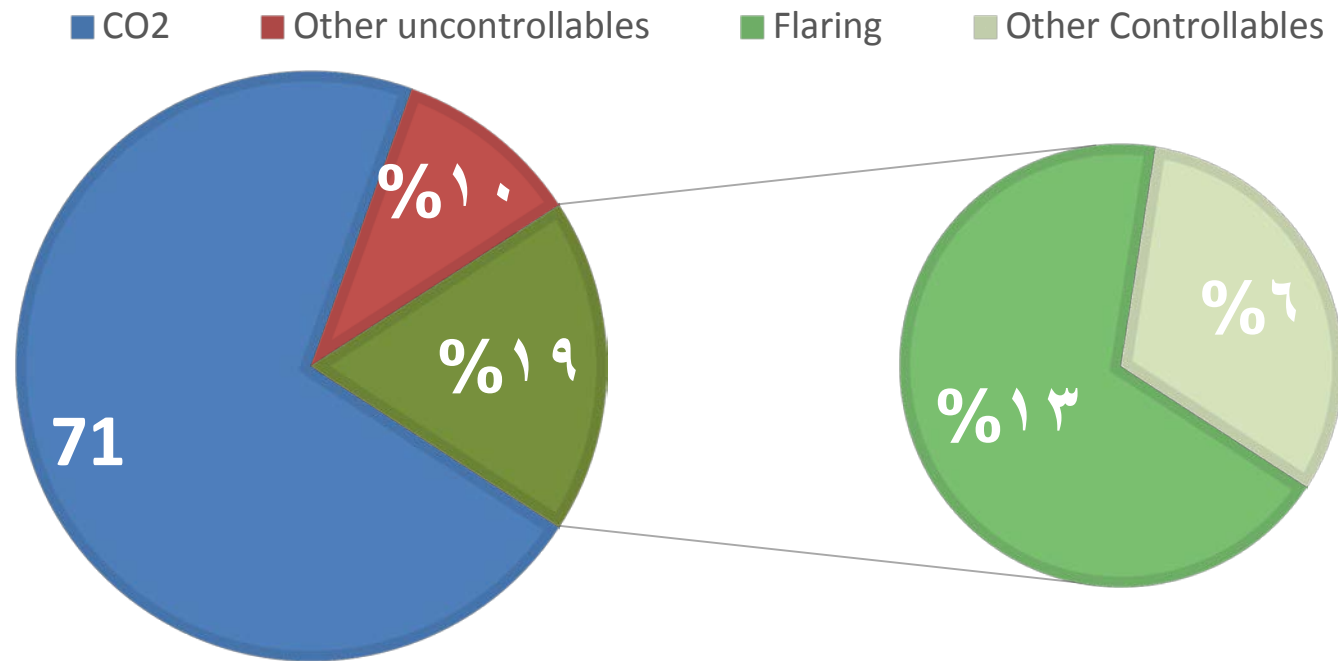
IR Camera – Multi-purpose tool that projects real-time picture showing temperature gradients.



Conclusion



LOSS BY BALANCE BREAKDOWNS



- ❑ 81% of the refinery reported loss found to be zero value, wherein 71% due to CO2 venting from HPU.
- ❑ Max Unaccountable Loss for MAA = 0.7% & MAB = 0.5%
- ❑ Totally new sources of losses have been identified.

Conclusion



- H/C Loss Book Value reduced by 81 %
- Improvement in physical HC Loss reported by Solomon since 2014 study.
- ⑩ KNPC are within the international companies practices. < 1%
- ⑩ KNPC reached the boundary for the first quartile for 2018 Solomon study with hc loss of about 0.2X%.



THANK YOU

